

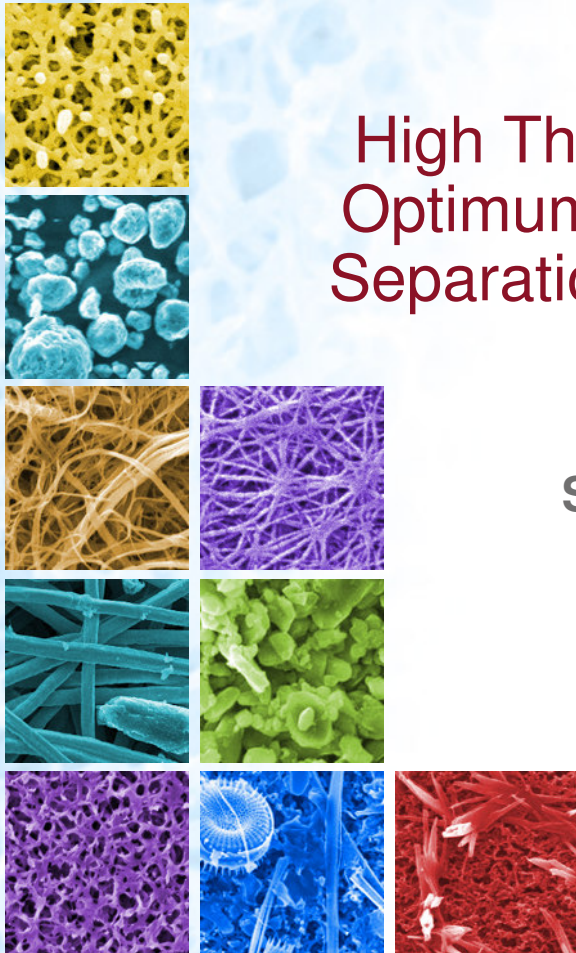


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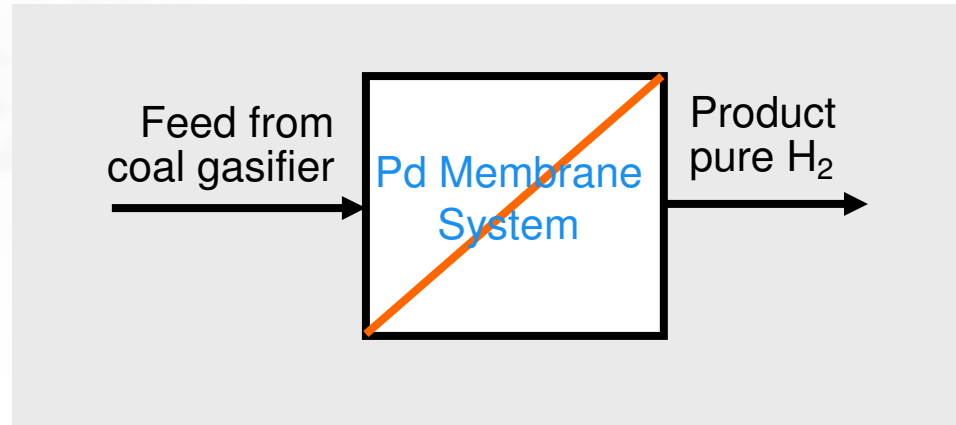
High Throughput Design of Ternary Pd Alloys for Optimum Sulfur / Carbon Resistance in Hydrogen Separation & Carbon Capture Membrane Systems

Scott D. Hopkins (PI), Hongbin Zhao (Presenter)

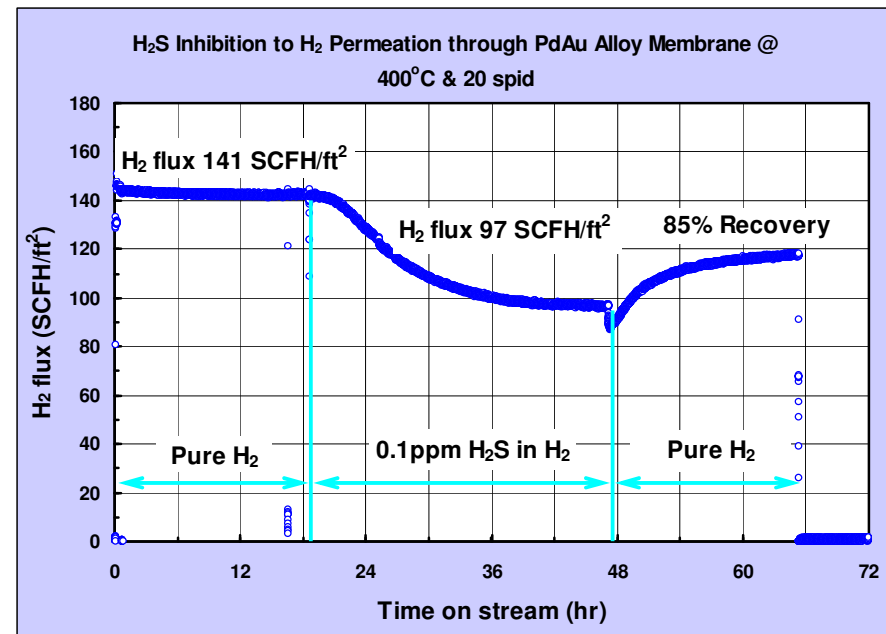
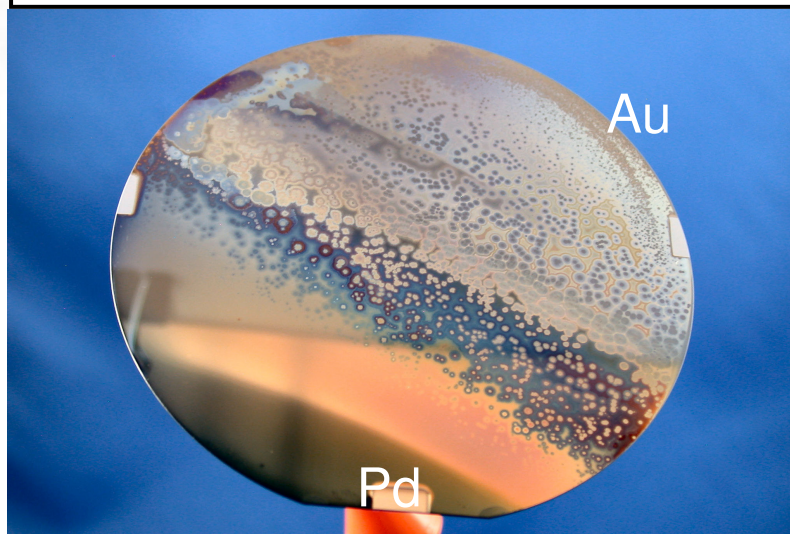
NETL CO₂ Capture Technology Meeting
Pittsburgh / July 9 – 12, 2012



Project Background: Problem and Approach

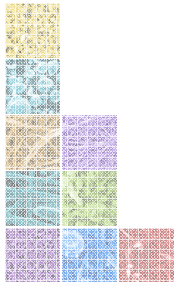


Coal Gas Corrosion Test of PdAu Alloy Film

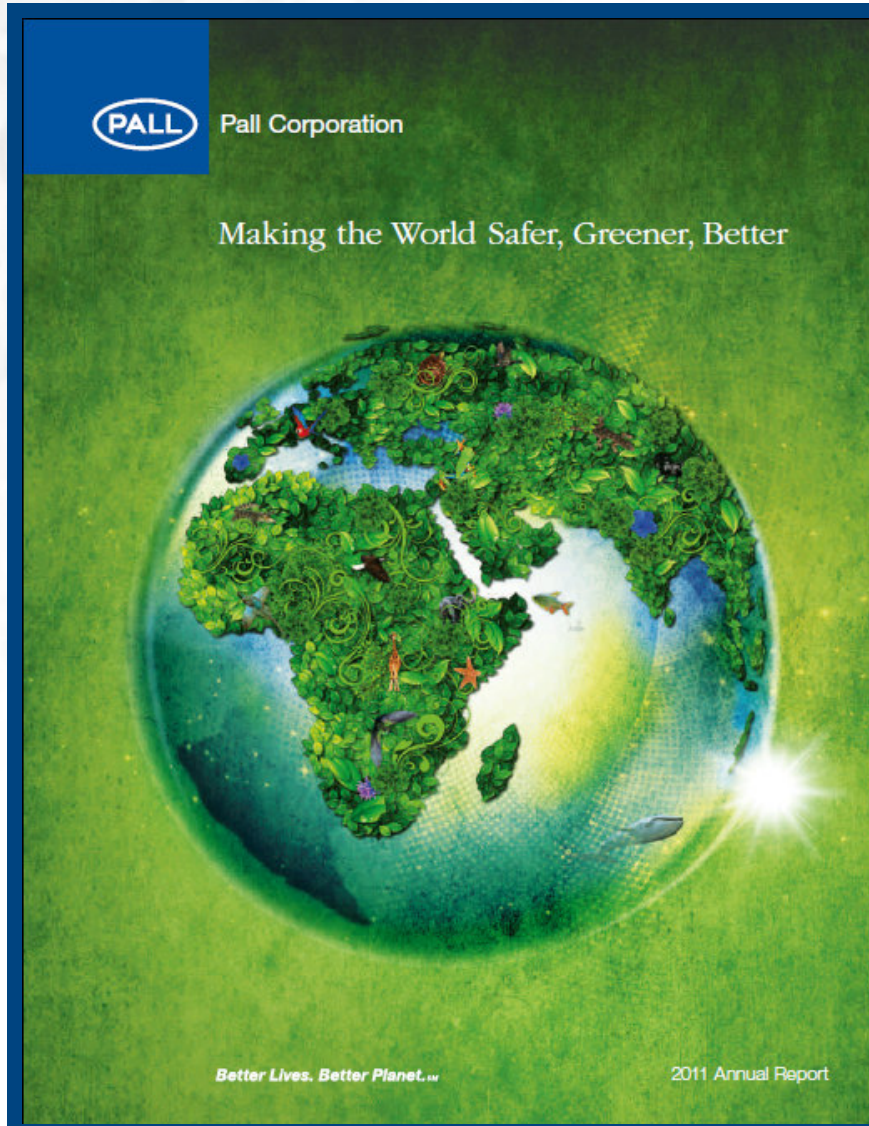


Outline

- Project overview
- Palladium membrane technology background
- Project progress as of 06/30/2012
- Future plans



Profile of Pall Corporation



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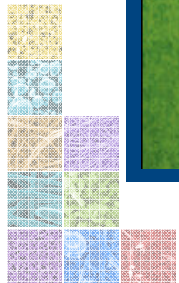


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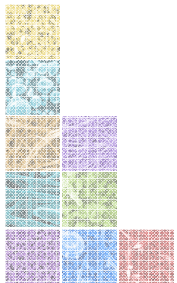
2011.04.01



Project Overview

Project Objectives

- Develop an economic, high temperature and pressure, hydrogen separation membrane system for CO₂ capture that resists moderate levels of contaminants, typical in gasified coal.
- Create an advanced palladium alloy for optimum hydrogen separation performance using combinatorial material methods for high-throughput screening, testing, and characterization.
- Demonstrate durability by long term testing of a pilot membrane module at a commercial coal gasification facility.
- Understand long term effects of the coal gasifier environment on the metallurgy of the membrane components.



Project Overview

Participants

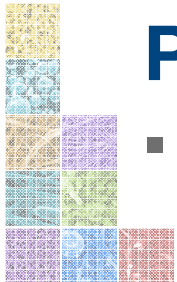
- Pall Corporation (project management, membrane fabrication and its scale-up technology, prototype membrane and module test)
- Cornell University (Combinatorial sample fabrication)
- Georgia Institute of Technology (Surface characterization of alloys)
- Oak Ridge National Laboratory (in-situ XRD of alloy phases)
- Southern Company (Long-term membrane module test)

Funding

- \$1,517,000 Total
- \$1,207,000 U.S. Department of Energy
- \$310,000 Cost Share

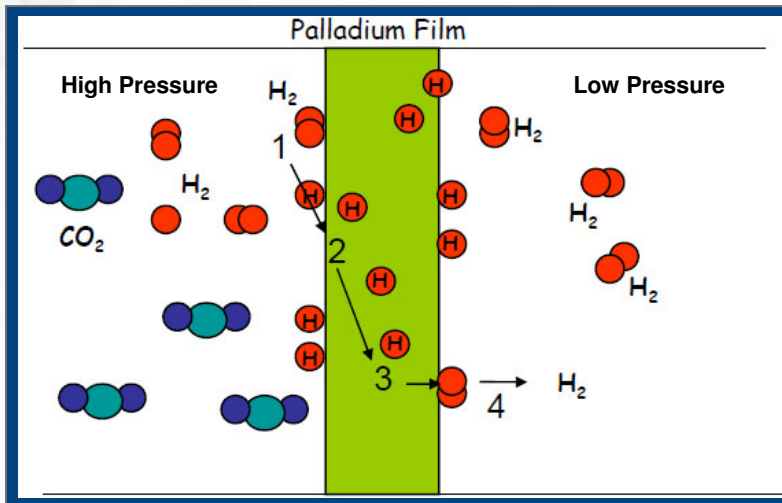
Performance Period

- Oct 1, 2009 to Sept 31, 2012 as proposed (three-year project)



How Palladium Membrane Works

Hydrogen Transport Through Palladium Film



- **H₂ dissociation on metal**
- **H dissolves into metal**
- **H diffuses through metal**
- **Recombination to form H₂**

Hydrogen Selectivity

- Infinite for defect-free palladium film

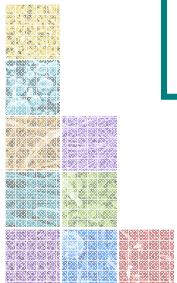
Hydrogen Flux Equation

- **Q**: H₂ permeability of palladium
- **L**: Thickness of palladium film
- **P_{H₂, feed}**: H₂ partial pressure in feed
- **P_{H₂, permeate}**: H₂ pressure in permeate

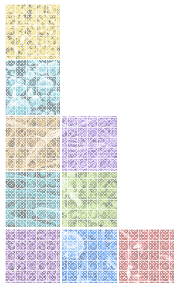
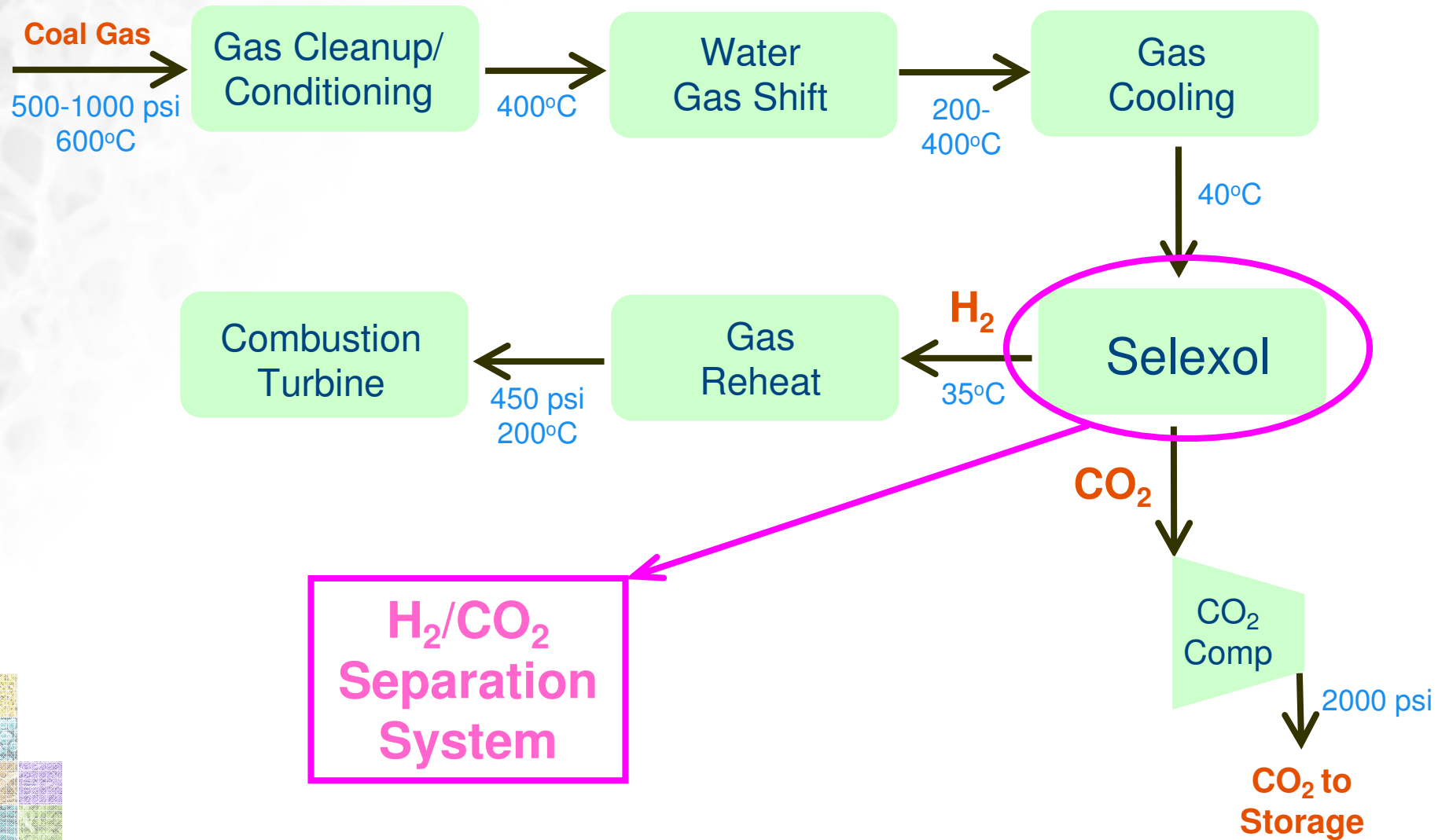
$$J_{H_2} = \frac{Q}{L} (P_{H_2, feed}^{0.5} - P_{H_2, permeate}^{0.5})$$

Design & Operating Considerations

- **High hydrogen permeable metal alloy**
- **Free membrane fouling materials**
- Thin membrane
- High membrane area
- High pressure
- High temperature



IGCC Power Plant with Pre-Combustion CO₂ Scrubbing



Palladium Membranes in IGCC Power Plants

Advantages

- No need for both upstream and downstream heat exchange and complex heat integration
- Reduce CO₂ compression costs
- Potential for integration with water gas shift in a single compact membrane reactor system

Coal Gas
500-1000 psi
600°C

Gas Cleanup/
Conditioning

400°C

Water
Gas Shift

200-
400°C

Palladium
Membrane

H₂ 400°C

Combustion
Turbine

CO₂

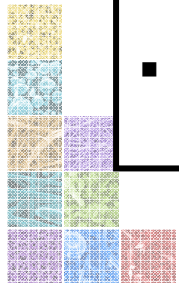
CO₂
Comp

CO₂ to
Storage

2000 psi

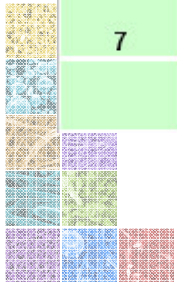
Challenges

- Severe poisoning of membrane surface by sulfur and others
- Inadequate, slow screening and testing methods for identification of new alloys



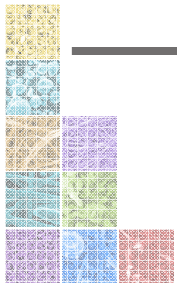
Project Schedule & Milestones

Task#	Project Milestone Description	2009		2010				2011				2012				
		Q3	Q4	Q1	Q2	Q3	Q4	Q1	Q2	Q3	Q4	Q1	Q2	Q3	Q4	
1	Project management and planning		→													
2	Literature and patent search		→													
	Milestone 1 Report demonstrating understanding of previous work			★												
3	Design and modeling of binary and ternary Pd alloys			→												
	Milestone 2 Report on use of combinatorial method					★										
4	Construct and test 15 cm ² active membrane area prototypes							→ 9 months no-cost extension								
	Milestone 3 Report on testing of small scale membranes									◆						
5	Scale up active membrane area from 15 to 75 cm ²								→							
	Milestone 4 Report on testing of scaled-up membranes										◆					
6	Construct and test a working membrane module										→					
	Milestone 5 Report on long-term performance of membranes													◆		
7	Provide complete analysis of relevant data sufficient of permit economic evaluatoin of the process											→				
	Milestone 6 Report on advancement necessary to commercialize membrane process														◆	



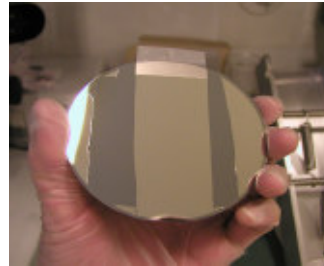
Progress and Current Status

Task	Timeline	Completion
<p>Task 4 Construct and test 15 cm² active surface area prototypes of novel Pd alloy membranes for use as high temperature, high pressure gas separation membranes under coal gasifier conditions</p> <ul style="list-style-type: none">Optimize process for making zirconia substrates suitable for each candidate Pd alloyFabricate best candidate palladium alloys into thin film membrane prototypes with 15-cm² active surface area over optimized zirconia substrateTest hydrogen separation performance of each best candidate alloy under coal gas conditions with trace amounts of impurities, including sulfur, for extended period	Oct 2010 to Sept 2011 (nine months of no cost extension due to limit to thin film deposition facility from subcontractor)	30%

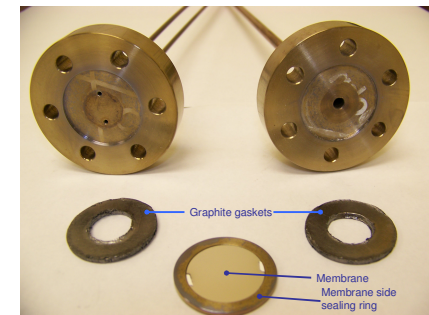


Combinatorial Pd Alloy Development Workflow

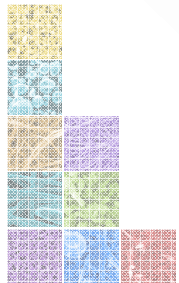
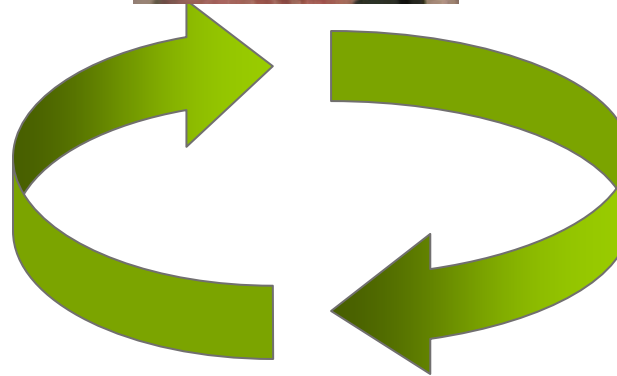
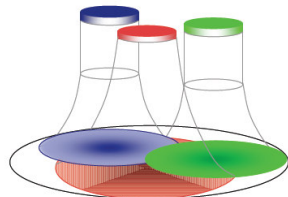
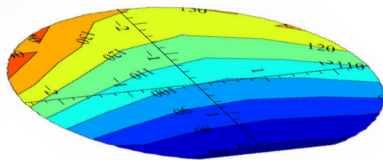
Freestanding Alloy Membrane Fabrication



Gas Permeation Performance Testing

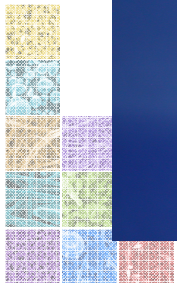
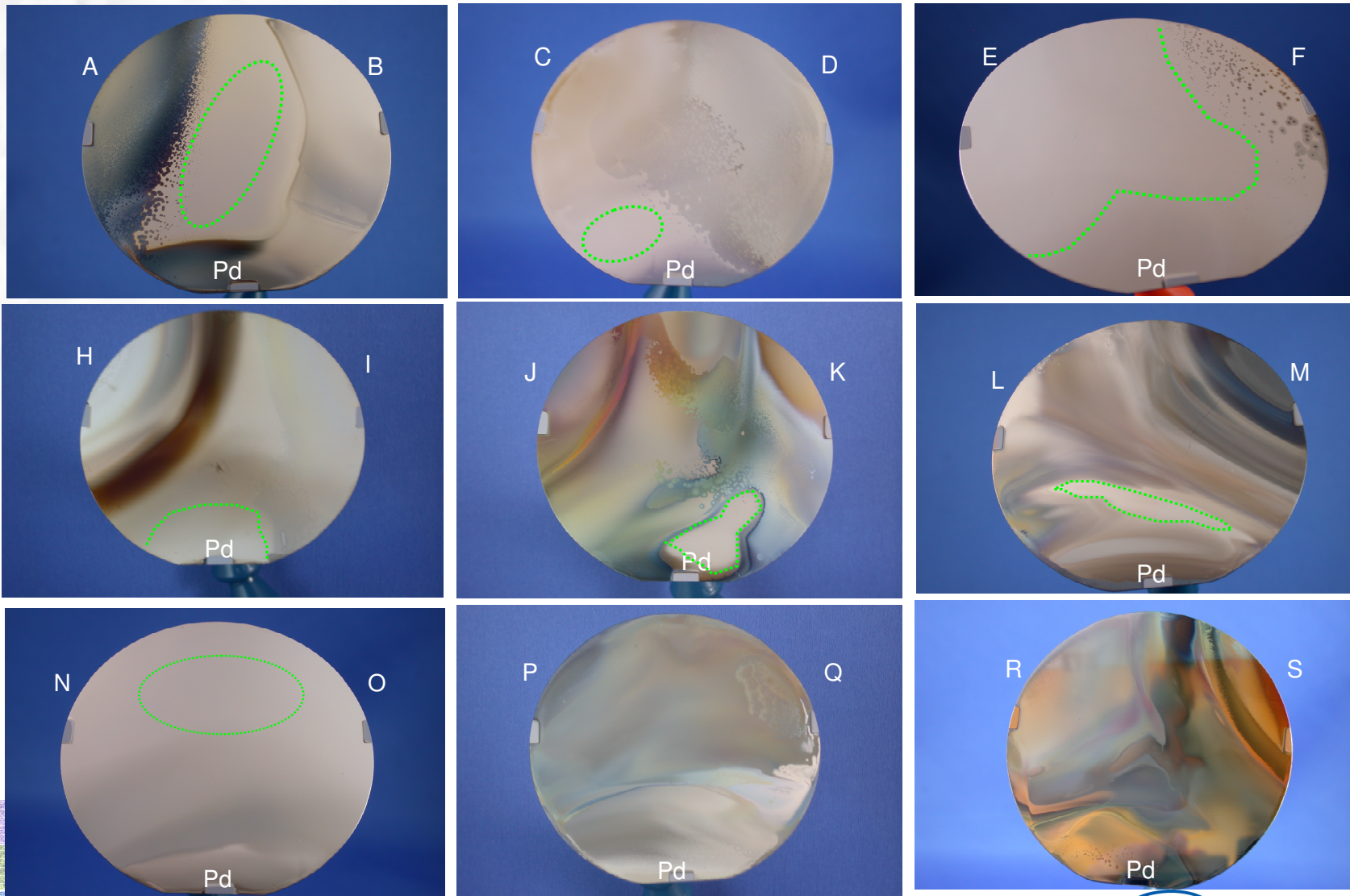


Combinatorial Discovery



Combinatorial Discoveries (Task #3)

No Corrosion Spots on Seven Ternary Composition Spreads

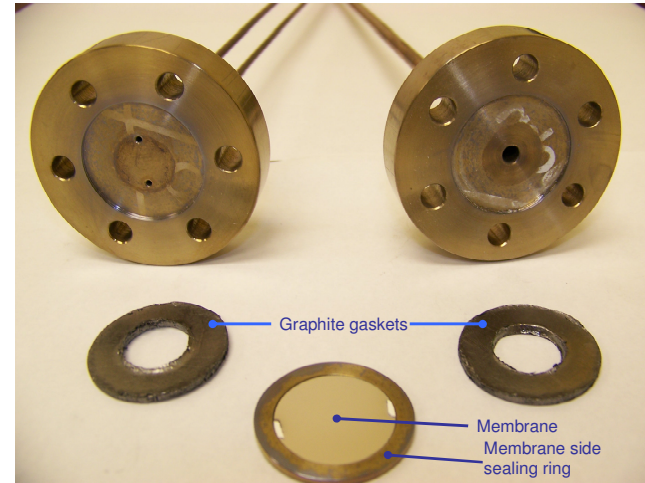


Pd Alloy Screening Test Protocol

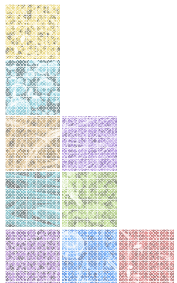
- Sulfur challenge test @ 400°C & 20 psid with a gas mixture of H₂S and H₂.
- Coal gas test @ 400°C & 200 psig (*coal gas composition H₂=17.6%, CO₂=17.9%, H₂O=2.6%, CO=2.6%, N₂=59.3%, H₂S up to 170 ppm)

*The composition of coal gas is provided by U.S. DOE / NCCC (site for future field test).

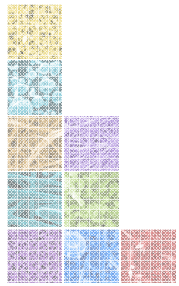
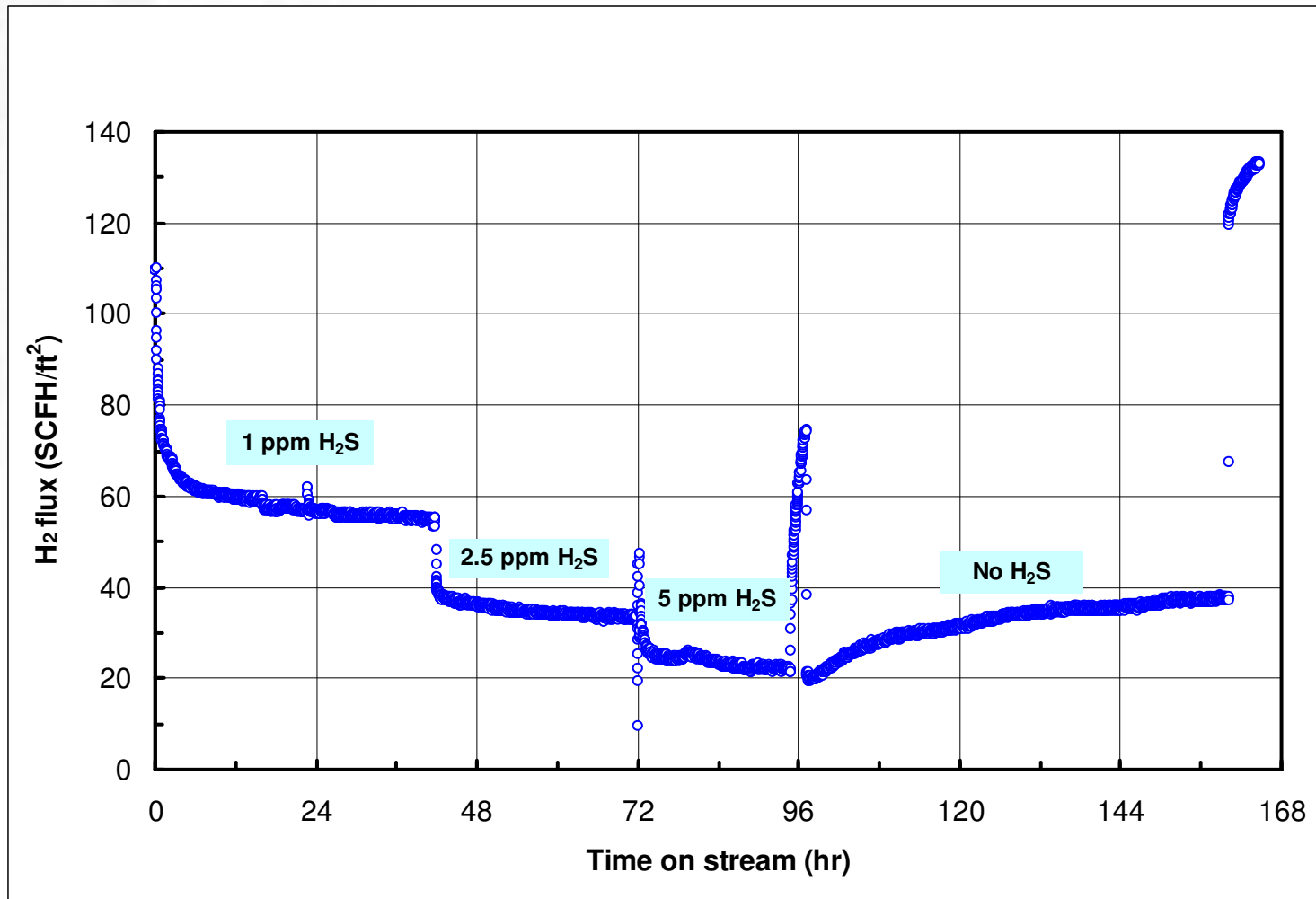
Gas Permeation Cell



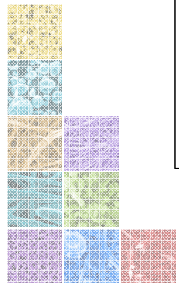
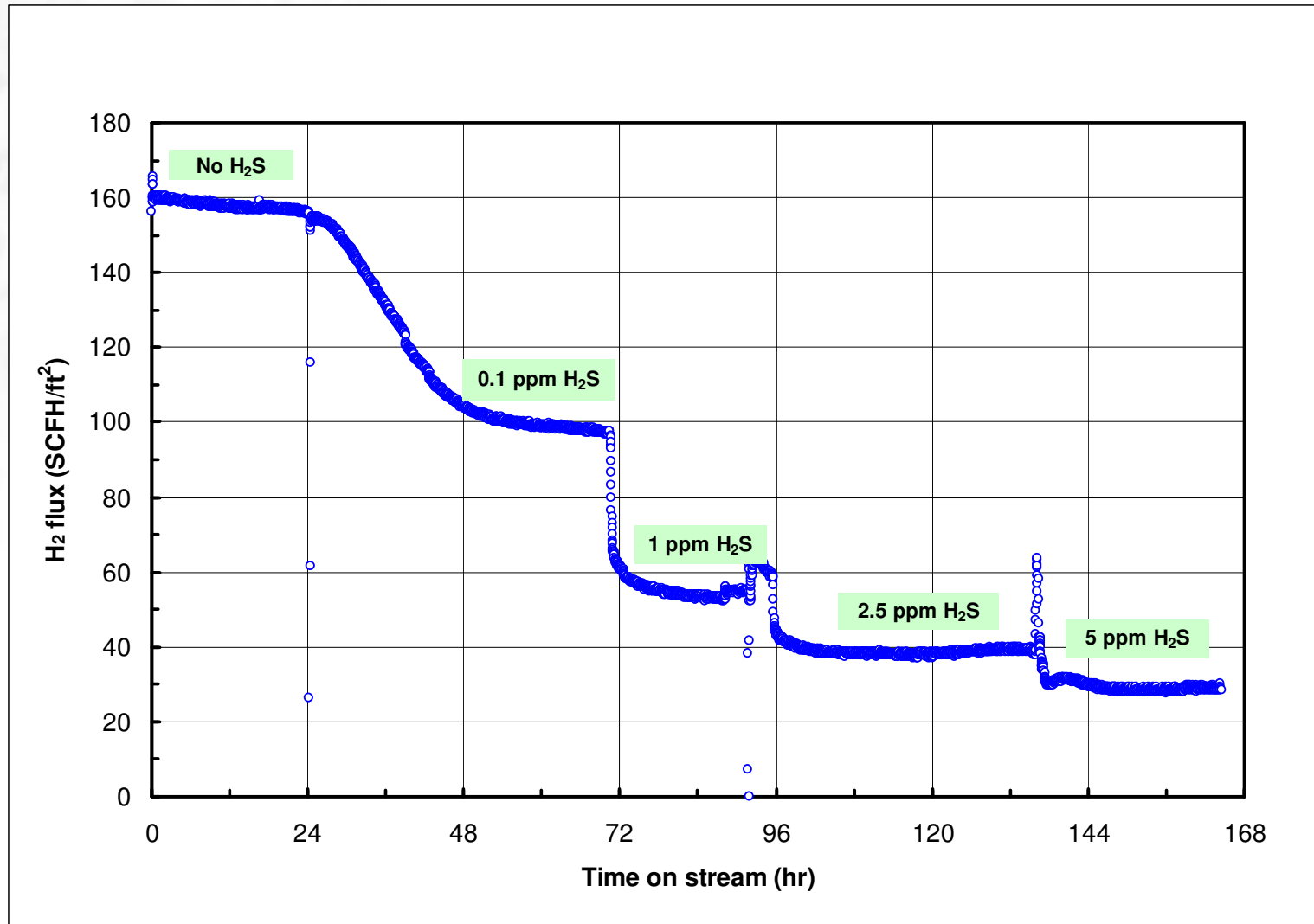
Gas Permeation Test Stand



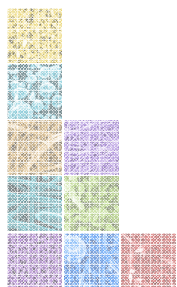
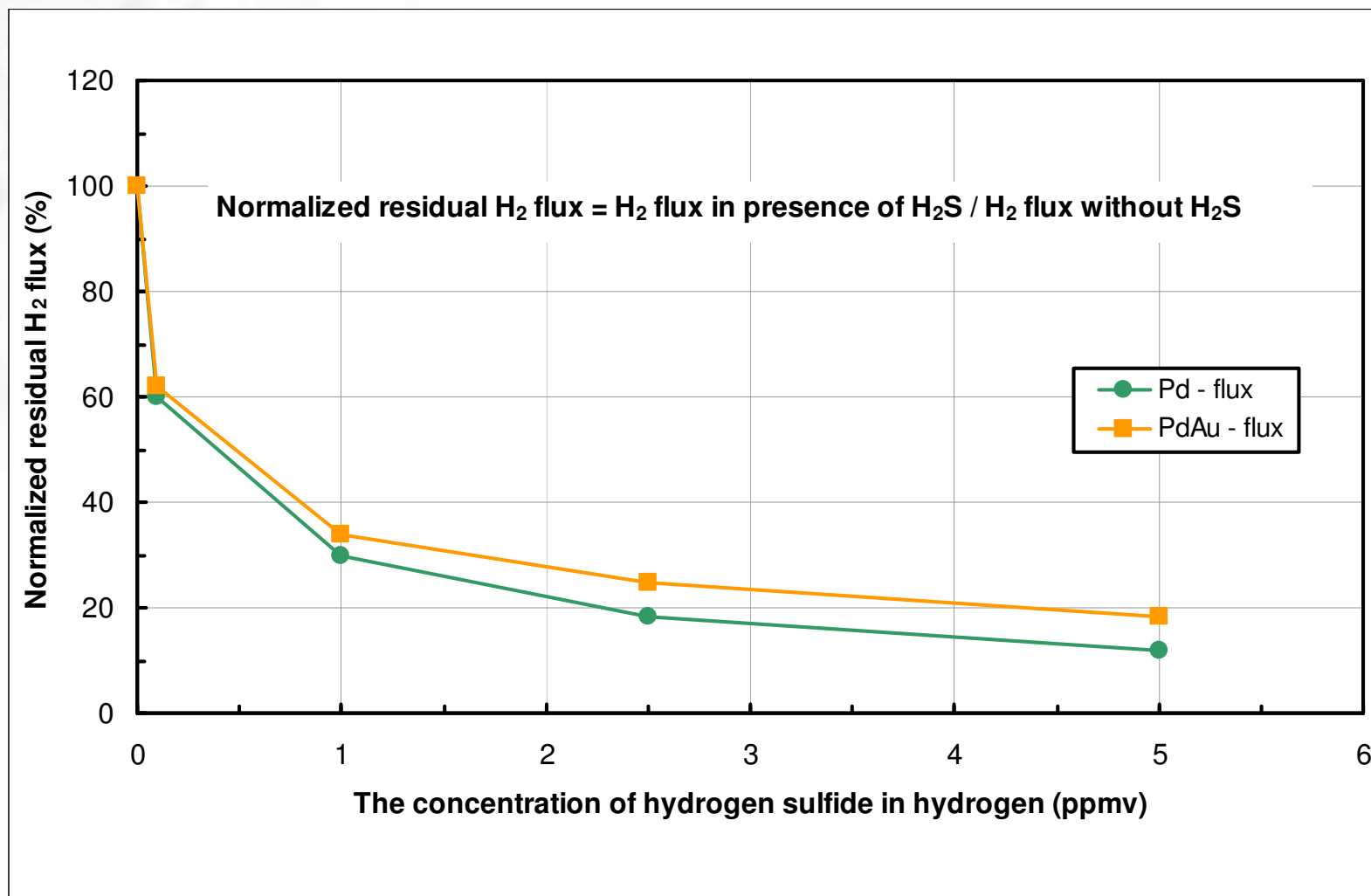
Sulfur Challenge Test on Pd Membrane



Sulfur Challenge Test on PdAu Alloy Membrane



Comparison of Sulfur Inhibition: Pd versus PdAu Alloy



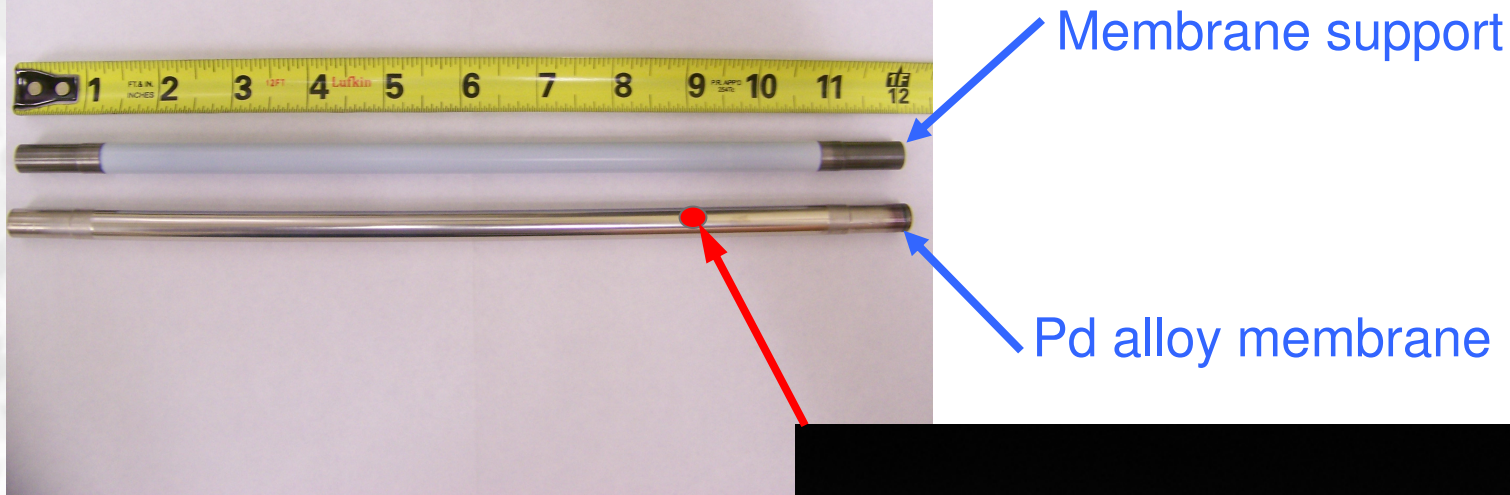
Plans to Complete Project

- Make flat sheet samples of alloy candidates selected from task #3 and test them in disc form to screen the best alloys based on sulfur tolerance level
- Select the best alloys and directly make full scale (active surface area 75 cm²) membrane element of novel palladium alloy prototypes
- Conduct 100-500 hour test on these 75 cm² samples in simulated coal gas with trace amounts of impurities including sulfur.
- Construct a working membrane module capable of extended service as a hydrogen separation system
- Conduct 500 hour relevant field test with real gasifier feed at U.S. DOE / NCCC
- Detailed process and economic modeling using field membrane performance data

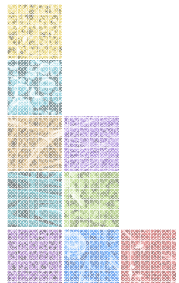
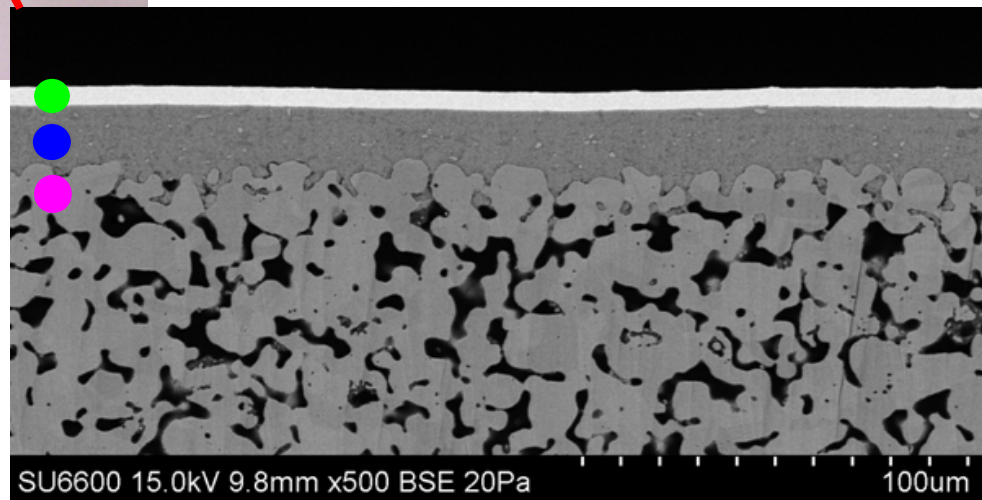


Pall's Capability in Palladium Membranes

Membrane Support & Pd Alloy Membrane Element

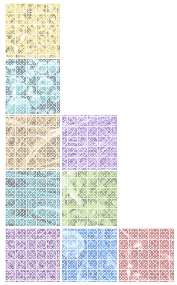
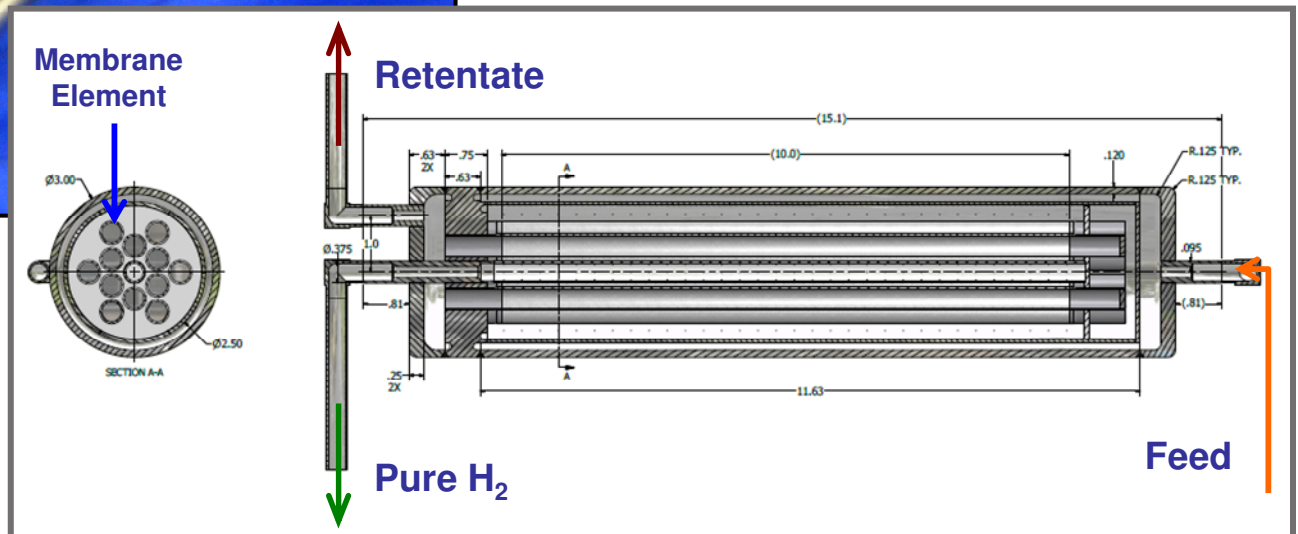


- Pd alloy top layer
- Ceramic intermediate layer
- Porous stainless steel substrate



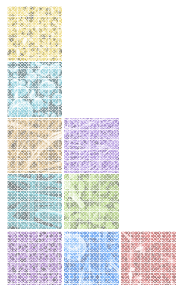
Pall's Capability in Palladium Membranes

5kw Palladium Alloy Membrane Module



Summary

- Discovered seven coal gas corrosion resistant ternary palladium alloy systems as candidates for sulfur tolerance level screening test
- Free-standing thin film deposition technique with uniform composition for ternary palladium alloy is being developed
- Capability for manufacturing and marketing of portable fuel cell size palladium alloy membrane module is fully established at Pall Corporation.
- Pall's capability above provides infrastructure for this project to complete and meantime success of this project will expand Pall's capability into other markets.



Acknowledgements

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